

Efficiency of *Pistia stratiotes* in treatment of municipal solid waste leachate in an upwards flow constructed wetland system

Mukesh Ruhela¹, Binod Kumar Jena¹, Sweta Bhardawaj¹, Rakesh Bhutiani² and Faheem Ahamad^{3*}

¹Department of Environmental Engineering (SITE), Swami Vivekanand Subharti University, Meerut 250 005, (UP), India

²Limnology and Ecological Modelling Lab. Department of Zoology and Environmental Science, Gurukula Kangri Vishwavidyalaya, Haridwar 249 404 (UK), India

³Keral Verma Subharti College of Sciences (KVSCOS), Swami Vivekanand Subharti University, Meerut 250 005, (UP), India.

(Received 17 March, 2020; Accepted 11 September, 2020)

ABSTRACT

Constructed wetlands are one of the effective treatment technologies that have been used to treat various kinds of wastewater and leachate and are very economical and cost-effective, simple and easy to operate, without any complex technology. The BOD₅/COD ratio of raw leachate was observed as low (0.27), indicating it as biodegradable leachate. That's why for the treatment of this leachate, CW's methods are used. The main objective of the present study is to assess the efficiency of CW's for the treatment of landfill leachate. To fulfill the objectives of the present study an upwards flow engineered wetland was constructed using gravel, sand and plant (*Pistia stratiotes*). The efficiency of CW's was assessed for 21 parameters such as TDS, COD, BOD, NH₄-N, Fluoride, TKN, and Heavy metals, etc. The maximum removal efficiency was observed in the case of BOD (97.58%) followed by COD (97.03%), Turbidity (87.09%) and Sulphate (85.89%) while minimum efficiency was observed in case of pH (8.24%). Due to the large removal efficiency observed in the present study and based on literature, it can be said that CW's methods would play a major role in the sustainable management of wastewater.

Key words: Constructed wetlands, Leachate, Municipal solid waste (MSW), Upward flow.

Introduction

Increasing urbanization, industrialization, and growing population and affluent lifestyle are the main causes of the increasing rate of solid waste generation (Chen *et al.*, 2013). Various methods adopted for solid waste management are incineration, pyrolysis, landfilling, etc. Leachate is the liquid that seeps through solid waste or another medium has extracts of dissolved or suspended material from it (Moravia *et al.*, 2013). Leachate quality de-

pends upon the type of waste (Schiopu and Gavrilescu, 2010). Both old leachate (methanogenic type) and fresh leachate (acidogenic type) possess different characteristics (Lak *et al.*, 2013; Hermosilla *et al.*, 2009; Abood *et al.*, 2014; Zazouli *et al.*, 2012). In rainy season leachate formation increased as the leachate formation occurs from moisture leached waste and rainwater percolation from degraded waste (Lak *et al.*, 2013; Singh and Tang, 2013; Venu *et al.*, 2014).

Leachate has high pH, TDS, TSS, Chlorides, Total

*Corresponding author's email: faheem.ahamad170390@gmail.com

nitrogen, Ammonical nitrogen, Cyanide, Fluoride, Ca^{+2} , Mg^{+2} , Nitrites, Fe^{+2} , Phenols, Arsenic, Nickel, lead, zinc, copper, Chromium, Cadmium, Mercury, BOD and COD (Paxeus, 2008; Klimiuk *et al.*, 2007) and toxic organic matters, which distribute among different particles with various sizes. Leachate formation occurs in three phases and these are- Aerobic phases, anaerobic phase, and methane phase. To confirm the potential dangers of leachates before discharging, its toxicity tests were performed on various test organisms as *Vibrio fisheri*, *Daphnia similis* and *Artemiasalina* (Silva *et al.*, 2004) and organic matter removal were assessed in the form of COD, BOD, and Ammonia. Biological methods were described as effective (Kang and Hwang, 2000; Ding *et al.*, 2001) for the treatment of young leachates (low ratio of BOD5/COD and low biodegradability), while for the treatment of old or partially stabilized leachates (high ratio of BOD5/COD and high biodegradability) physicochemical processes were described as effective (Ntampou *et al.*, 2005). Biological methods investigated and used are: UASB, activated sludge, stabilization ponds, bio discs, trickling filters and SBR (Agdag and Sponza, 2005), while physicochemical technologies used are coagulation, flocculation, sedimentation, reverse osmosis, micro and ultrafiltration, ammonia stripping and advanced oxidation processes (Zouboulis *et al.*, 2004; Zhang *et al.*, 2005).

Implementation of the above discussed biological and physicochemical process of leachate treatments requires high operation costs and skilled labor but the economy of developing countries such as India is not so good to support these expensive treatments (Chiemchaisri *et al.*, 2009). Taking the above discussion into account and the serious consequences of the groundwater pollution problem from leachate, the landfill leachate treatment problems are urgent to solve. There is an urgent need to work with systems more flexible and low cost both in investment, operation, and maintenance. Leachate treatment with constructive wetland is the system applicable to the entire situation discussed above.

Natural wetland is an area consisting of soil, plant, and water where the soil is covered by water or saturated with moisture such as marsh, swamp or bog while constructed wetland is defined as engineer-made equivalent to natural wetlands and designed to reduce and mitigate the pollution level from wastewater as occurred in natural wetlands (Kumar and Choudhary, 2018). Constructed wet-

land consists of gravel, water or shallow pond, soil, aquatic plant or macrophyte and microorganism (Saeed and Sun, 2012). For developing countries and remote sites with a small community, constructed wetlands are very useful for leachate treatment and possess higher efficiency (Bakhshodeh *et al.*, 2017; Gajewska *et al.*, 2015).

In comparison to conventional treatment processes, constructed wetlands are easy in operation and low cost in maintenance and offer an alternative way of leachate treatment (Kumar and Choudhary, 2018; Akinbile *et al.*, 2012; Choudhary *et al.*, 2011). These are a combination of physical, chemical and biological processes and act as a biological filter. Vertical flow constructed wetlands (VF CWs) are more efficient than other wetlands. VF CWs requires a very small space for its operation. They depend upon various processes like filtration, sedimentation, volatilization, precipitation, adsorption, etc. Constructed wetlands system is widely applied for the purification of domestic waste, stormwater runoff, and industrial effluent. In the present study, we worked on the upward flow constructed.

The leachate was collected from Bawana Dumping Yard, Delhi, operated since 2011. Narela-Bawanais the first scientific landfill site of city Delhi. Approximately 1300 metric tonnes of solid waste are continuously processed to obtain refused derived fuel (RDF), manure and other recyclable items. Delhi spread over 1483 square Km area and is situated in North India at an altitude of 293 m above mean sea level. Delhi (2nd rank occupier in population among all Indian metropolitan cities), is estimated to generate about 10500 metric tons of MSW daily. Per capita generation of solid waste in Delhi ranged from 550 to 600 gm/d. The waste processing capacity of Delhi is 6,100 tonnes per day (TPD), with the help of three incineration plants and two centralized composting units. Approximately 4,600 TPD of waste from commercial, industrial and residential areas is disposed of in three dumping sites of Delhi, i.e. Okhla, Bhalswa and Ghazipur. The Narela-Bawana MSW site is constructed in different phases. Currently, it is processing 2000 tonnes/day of waste for processing, disposal, and waste to energy conversion. The site is producing 24MW electricity from waste. It has an area of approximately 100ha, including ballistic separators, including Refuse Derived Fuel (RDF) trammels, Compost Plant and waste to the energy power plant.

Materials and Methods

The leachate sample was collected from the solar evaporation pond (SEP) in the center of the MSW landfill of Bawana. Leachate sample was collected in 20 liters plastic containers (previously acidified with HCL). Some parameters were analyzed at the site while for the analysis of the rest of the parameters and experiment, the sample was transported to the laboratory immediately. All the samples were analyzed following the standards methods (APHA, 2012; Khanna and Bhutiani, 2008; Trivedy and Goel, 1986).

Plant species and experimental setup

For the experiment, the macrophyte (water lettuce also called pistia) was selected. Pistia is one of the genera of aquatic plants in the arum family, *Araceae*. The other name of *Pistia stratiotes*, are water cabbage, water lettuce, Nile cabbage, or shellflower. The selected plant was collected from the nearby village ponds and then their root was washed after that, the plant was cultivated in the artificial pond. In artificial ponds, the plants grow and stabilize their population. The experiment was conducted in three phases as phase 1, phase 2 and phase 3. Phase 1 is associated with the collection and stabilization of the plant population. Phase 2 is associated with the optimization of experimental factors (HRT, SRT, the width of sand and gravel bed and diameter of gravel) while phase 3 is the actual experiment phase. Before phases 1, 2 and 3, the leachate was diluted with groundwater and then aeration was performed to reduce the concentration of ammonia and to improve the C/N ratio (Smaoui *et al.*, 2019). The wetland was constructed in horizontal design. The layers consisted of 15 cm of 0.3–2 mm diameters of sand and, 20 cm of 5–15 mm diameter semi-coarse gravel and 30 cm of 15–25 mm diameter coarse gravel. The uniformity coefficient for the sand is 3.55, for semi-coarse gravel 1.67 and coarse

gravel layers were 1.37.

Calculation of pollutant removal efficiency

The mechanism of pollutant removal in constructed wetlands (CWs) involve physical treatment i.e. filtration through soil layer, adsorption on the surface of media used, sedimentation, and chemical treatment, i.e. precipitation and oxidation-reduction, and bio-treatment, i.e. uptake of pollutant by plant and bio-degradation with the help of micro-organism (Choudhary *et al.*, 2011; Sauba, 2015) (Table 1). The water is treated primarily before the experiment to suspended matter which can clog the experimental system (Pedescoll *et al.*, 2013). Large gravels create a film for producing bacterial growth. The mode of feeding (i.e. continuous, batch or intermittent) wastewater may affect the treatment efficiency by influencing oxygen transfer, redox conditions, and diffusion of pollutants in the wetland system.

The removal efficiency was obtained using the following equation:-

$$\text{Percentage removal} = \frac{X_i - X_f}{X_i} \times 100$$

Where X_i and X_f refer to the initial and final concentration of the particular parameters.

Results

The samples (Raw leachate, Diluted leachate and treated leachate) collected during the study period was analyzed for the following parameters as pH, TSS, TDS, TS, Chloride, Total Kjeldahl Nitrogen (TKN), Ammonical nitrogen ($\text{NH}_4\text{-N}$), Fluoride, Nitrites, Total Phosphorous (T-Phosphorous), Sulphate, DO, BOD, COD and heavy metals (Nickel, Lead, Copper, Iron, and Cadmium) and the results of all the parameters were presented in the Table from 1 to 3.

The average turbidity of the raw leachate was

Table 1. Treatment Processes in Constructed Wetlands (Kumar and Choudhary, 2018).

| Parameter | Removal mechanism |
|--------------------|--|
| Suspended solids | Sedimentation and filtration |
| Dissolved Organics | Aerobic and anaerobic microbial degradation, phyto-degradation, phyto-volatilization, and plant uptake |
| Phosphorus | Plant uptake and matrix sorption |
| Nitrogen | Ammonification, microbial nitrification, plant uptake, denitrification, matrix adsorption |
| Metals | Sedimentation, filtration, adsorption, precipitation, and plant uptake |

found 116.80 ± 13.68 (Ranged from 96 NTU to 136 NTU) while after dilution the turbidity of the leachate was found 57.30 ± 5.54 (Ranged from 48 NTU to 67 NTU). After treatment with the constructed wetlands, the turbidity of the leachate was found 7.40 ± 1.8 (Ranged from 5 NTU to 10 NTU). The average conductivity of the raw leachate was found 12270.10 ± 413.77 (Ranged from $11920.9 \mu\text{S}/\text{Cm}$ to $13113.4 \mu\text{S}/\text{Cm}$) while after dilution the conductivity of the leachate was found 9000.6 ± 336.5 (Ranged from $8425.4 \mu\text{S}/\text{Cm}$ to $9771.6 \mu\text{S}/\text{Cm}$). After treatment with the constructed wetlands, the conductivity of the leachate was found 1803.1 ± 88.5 (Ranged from $1712.4 \mu\text{S}/\text{Cm}$ to $2015.4 \mu\text{S}/\text{Cm}$).

The average total dissolved solids (TDS) of the raw leachate was found 8221.10 ± 272.22 (Ranged from $7987 \text{mg}/\text{L}$ to $8786 \text{mg}/\text{L}$) while after dilution the TDS of the leachate was found 6030.40 ± 225.47 (Ranged from $5645 \text{mg}/\text{L}$ to $6547 \text{mg}/\text{L}$). After treatment with the constructed wetlands, the TDS of the leachate was found 1192.40 ± 48.7 (Ranged from $1120 \text{mg}/\text{L}$ to $1278 \text{mg}/\text{L}$). The average total suspended solids (TSS) of the raw leachate was found 205.90 ± 20.01 (Ranged from $180 \text{mg}/\text{L}$ to $245 \text{mg}/\text{L}$)

while after dilution the TSS of the leachate was found 147.00 ± 22.7 (Ranged from $121 \text{mg}/\text{L}$ to $183 \text{mg}/\text{L}$). A more or less similar characterization of leachate was also found by Gusman *et al.*, 2015. After treatment with the constructed wetlands, the TSS of the leachate was found 43.30 ± 6.6 (Ranged from $35 \text{mg}/\text{L}$ to $56 \text{mg}/\text{L}$). The average total solids (TS) of the raw leachate was found 8427.00 ± 271.97 (Ranged from $8208 \text{mg}/\text{L}$ to $8975 \text{mg}/\text{L}$) while after dilution the TS of the leachate was found 6177.40 ± 230.52 (Ranged from $5767 \text{mg}/\text{L}$ to $6990 \text{mg}/\text{L}$). After treatment with the constructed wetlands, the TS of the leachate were found 1344.00 ± 35.9 (Ranged from $1300 \text{mg}/\text{L}$ to $1410 \text{mg}/\text{L}$).

The average pH of the raw leachate was found 7.98 ± 0.14 (Ranged from 7.8 to 8.2) while after dilution the pH of the leachate was found 7.82 ± 0.12 (Ranged from 7.56 to 7.96). A more or less similar trend in pH was observed by Gotvajn *et al.*, 2009. After treatment with the constructed wetlands, the pH of the leachate was found 7.18 ± 0.09 (Ranged from 7.07 to 7.32). The average biochemical oxygen demand (BOD) of the raw leachate was found 3421.50 ± 433.58 (Ranged from $2818 \text{mg}/\text{L}$ to $4103 \text{mg}/\text{L}$) while after dilution the BOD of the leachate

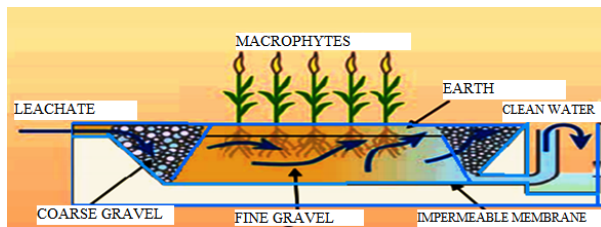


Fig. 1. Showing the Adapted design for the present study (Adapted from UNEP, 2003)



Fig. 2. Leachate collection site (Solar Evaporation Pond)

Table 1. Showing Physical characteristics of Raw diluted leachate and Treated leachate.

| SPL/PMS | Turbidity (NTU) | | Conductivity ($\mu\text{S}/\text{cm}$) | | TDS (mg/L) | | TSS (mg/L) | | TS (mg/L) | |
|---------|-----------------|-----|--|--------|------------|--------|------------|------|-----------|------|
| | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW |
| SN-1 | 67 | 9 | 8425.4 | 1813.5 | 5645 | 1220 | 122 | 35 | 5767 | 1300 |
| SN-2 | 56 | 8 | 8804.5 | 1765.8 | 5899 | 1180 | 158 | 45 | 6057 | 1345 |
| SN-3 | 61 | 9 | 8956.7 | 1876.9 | 6001 | 1278 | 142 | 43 | 6143 | 1365 |
| SN-4 | 61 | 10 | 9138.8 | 2015.4 | 6123 | 1250 | 183 | 56 | 6306 | 1360 |
| SN-5 | 60 | 5 | 8934.3 | 1723.8 | 5986 | 1170 | 133 | 41 | 6119 | 1350 |
| SN-6 | 57 | 5 | 9771.6 | 1745.4 | 6547 | 1120 | 143 | 47 | 6690 | 1410 |
| SN-7 | 59 | 6 | 8935.8 | 1800 | 5987 | 1206 | 177 | 51 | 6164 | 1370 |
| SN-8 | 52 | 8 | 8922.4 | 1797.8 | 5978 | 1200 | 121 | 36 | 6099 | 1300 |
| SN-9 | 52 | 8 | 8977.6 | 1712.4 | 6015 | 1160 | 165 | 40 | 6180 | 1300 |
| SN-10 | 48 | 6 | 9138.8 | 1780 | 6123 | 1140 | 126 | 39 | 6249 | 1340 |
| AV | 57.3 | 7.4 | 9000.6 | 1803.1 | 6030.4 | 1192.4 | 147 | 43.3 | 6177.4 | 1344 |
| SD | 5.5 | 1.8 | 336.5 | 88.5 | 225.5 | 48.7 | 22.7 | 6.6 | 230.5 | 35.9 |

was found 1615.10±77.46 (Ranged from 1467mg/ L to 1725 mg/L). After treatment with the constructed wetlands, the BOD of the leachate was found 39.10±11.97 (Ranged from 25 mg/L to 56 mg/L). The average chemical oxygen demand (COD) of the raw leachate was found 12580.10±635.40 (Ranged from 11899 mg/L to 1410 mg/L). A more or less similar COD in Raw leachate was also observed by several researchers (Ohwoghere Asumaand Aweto, 2013), while after dilution the COD of the leachate was found 6274.50±556.15 (Ranged from 5654mg/ L to 7324 mg/L). A more or less similar observation was obtained by Singh *et al.*, 2016. After treatment with the constructed wetlands, the COD of the leachate was found 186.30±24.18 (Ranged from 160 mg/L to 223 mg/L).

The average Total Kjeldahl Nitrogen (TKN) of the raw leachate was found 246.50±21.20 (Ranged from 225 mg/L to 297mg/L) while after dilution the TKN of the leachate was found 141.60±14.12 (Ranged from 125 mg/L to 165 mg/L). After treatment with the constructed wetlands, the TKN of the leachate was found 33.40±4.43 (Ranged from 26mg/ L to 38 mg/L). The average Ammonical nitrogen (NH₄⁺-N) of the raw leachate was found 116.40±18.90 (Ranged from 93 mg/L to 156 mg/L) while after dilution the NH₄⁺-N of the leachate was found 55.40±11.47 (Ranged from 40 mg/L to 76 mg/L). After treatment with the constructed wetlands, the NH₄⁺-N of the leachate was found 23.60±3.63 (Ranged from 18 mg/L to 30 mg/L).

The average chloride of the raw leachate was found 2787.30±131.90 (Ranged from 2650mg L/ to 3017 mg/L) while after dilution the chloride of the leachate was found 1295.50±79.02 (Ranged from 145 mg/L to 1678 mg/L). After treatment with the constructed wetlands, the chloride of the raw leachate was found 504.30±21.68 (Ranged from 485 mg/L to 543 mg/L). The average nitrates of the raw leachate were found 41.05±3.18 (Ranged from 35.67 mg/L to 45.8mg/L) while after dilution the nitrates of the leachate were found 23.25±0.82 (Ranged from 21.98 mg/ L to 24.67 mg/ L). Our results are in agreement with Boumechhour *et al.*,2016. After the treatment with constructed wetlands, the nitrate of the leachate was found 8.09±0.56 (Ranged from 7.45 mg/L to 9.12 mg/L). The average fluoride of the raw leachate was found 1.48±0.16 (Ranged from 1.27 mg/v to 1.76 mg/L) while after dilution the fluorides of the leachate were found 0.68±0.07 (Ranged from 0.78 mg/L to 0.97 mg/L). After the

Table 2. Showing Chemical characteristics of Raw diluted leachateand Treated leachate.

| SPL/PMS | pH | | BOD (mg/L) | | COD (mg/L) | | TKN (mg/L) | | NH ₄ ⁺ -N (mg/L) | | Chloride (mg/L) | | Nitrates (mg/L) | | Fluorides (mg/L) | | TP (mg/L) | | Sulphate (mg/L) | |
|---------|-----|-----|------------|------|------------|-------|------------|------|--|------|-----------------|-------|-----------------|------|------------------|------|-----------|-----|-----------------|------|
| | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW |
| SN-1 | 7.8 | 7.3 | 1545 | 27 | 6134 | 189 | 134 | 34 | 45 | 20 | 1543 | 512 | 23.67 | 8.97 | 0.89 | 0.28 | 12.5 | 4.6 | 22.3 | 3.5 |
| SN-2 | 7.8 | 7.3 | 1634 | 51 | 6578 | 213 | 156 | 38 | 40 | 18 | 1456 | 489 | 22.34 | 7.89 | 0.86 | 0.25 | 14.1 | 5.1 | 24.5 | 2.9 |
| SN-3 | 7.9 | 7.1 | 1600 | 38 | 5767 | 167 | 128 | 26 | 55 | 23 | 1450 | 490 | 23.5 | 8.09 | 0.93 | 0.32 | 13.6 | 4.8 | 25.1 | 4.6 |
| SN-4 | 7.9 | 7.1 | 1614 | 49 | 5987 | 170 | 165 | 38 | 40 | 20 | 1678 | 543 | 24.67 | 9.12 | 0.78 | 0.24 | 13.9 | 3.5 | 22.1 | 4.1 |
| SN-5 | 7.6 | 7.2 | 1725 | 56 | 7234 | 223 | 160 | 37 | 56 | 24 | 1545 | 510 | 23.7 | 8.12 | 0.87 | 0.26 | 13.2 | 3.6 | 24.1 | 3.2 |
| SN-6 | 7.8 | 7.2 | 1467 | 25 | 5654 | 160 | 143 | 35 | 67 | 26 | 1500 | 496 | 21.98 | 7.45 | 0.97 | 0.38 | 14.8 | 4.1 | 22.3 | 3.8 |
| SN-7 | 7.7 | 7.1 | 1598 | 28 | 5878 | 165 | 125 | 28 | 55 | 25 | 1480 | 485 | 23.89 | 8.24 | 0.78 | 0.25 | 15.7 | 4.7 | 21.9 | 2.5 |
| SN-8 | 7.9 | 7.1 | 1580 | 26 | 5934 | 168 | 130 | 28 | 60 | 27 | 1500 | 492 | 22.78 | 7.85 | 0.81 | 0.25 | 13.9 | 3.9 | 22.7 | 3.4 |
| SN-9 | 7.9 | 7.1 | 1678 | 41 | 6456 | 189 | 140 | 35 | 76 | 30 | 1656 | 540 | 23.45 | 7.56 | 0.95 | 0.36 | 13.7 | 3.9 | 21.9 | 2.3 |
| SN-10 | 7.9 | 7.2 | 1710 | 50 | 7123 | 219 | 135 | 35 | 60 | 23 | 1487 | 486 | 22.54 | 7.65 | 0.79 | 0.25 | 14.9 | 4.5 | 22.8 | 2.1 |
| AV | 7.8 | 7.2 | 1615.1 | 39.1 | 6274.5 | 186.3 | 141.6 | 33.4 | 55.4 | 23.6 | 1529.5 | 504.3 | 23.3 | 8.1 | 0.9 | 0.3 | 14.0 | 4.3 | 22.9 | 3.2 |
| SD | 0.1 | 0.1 | 77.5 | 11.9 | 556.2 | 24.2 | 14.1 | 4.4 | 11.5 | 3.6 | 79.0 | 21.7 | 0.8 | 0.6 | 0.1 | 0.1 | 0.91 | 0.5 | 1. | 0.81 |

SPL- Sampling
 PMS- Parameters
 BOD-Biochemical Oxygen Demand
 COD-Chemical Oxygen Demand
 TKN-Total KjeldahlNitrogen
 NH₄⁺-N- Ammonical Nitrogen
 TP-Total Phosphorus

treatment with constructed wetlands, the fluoride of the raw leachate was found 0.28 ± 0.05 (Ranged from 0.24 mg/ L to 0.38 mg/ L). The average phosphorous (T-Phosphorous) of the raw leachate was found 32.60 ± 1.99 (Ranged from 28.9 mg/ L to 35.7 mg/L) while after dilution the total phosphorous of the leachate was found 14.03 ± 0.91 (Ranged from 12.50 mg/L to 15.70 mg/ L l). After treatment with the constructed wetlands, the total phosphorous of the raw leachate was found 4.27 ± 0.54 (Ranged from 3.50 mg/L to 5.10 mg/L). The average sulfate of the raw leachate was found 39.21 ± 1.50 (Ranged from 36.9 mg/L to 41.2 mg/L) while after dilution the sulfate of the leachate was found 22.97 ± 1.16 (Ranged from 21.9 mg/ L to 25.1 mg/ L). Our results are in agreement with Agbozu *et al.*, 2015. After treatment with the constructed wetlands, the sulfate of the raw leachate was found 3.24 ± 0.81 (Ranged from 2.1 mg/ L to 4.6 mg/ L).

The average nickel (Ni) of the raw leachate was found 0.43 ± 0.03 (Ranged from 0.38 mg/L to 0.49 mg/ L) while after dilution the nickel of the leachate was found 0.14 ± 0.03 (Ranged from 0.11 mg/L to 0.18 mg/ L). After treatment with the constructed wetlands, the nickel of the raw leachate was found 0.04 ± 0.01 (Ranged from 0.02 mg/L to 0.06 mg/L). The average lead (Pb) of the raw leachate was found 0.04 ± 0.01 (Ranged from 0.032 mg/L to 0.055 mg/L) while after dilution the lead of the leachate was found 0.03 ± 0.00 (Ranged from 0.02 mg/L to 0.03 mg/L). After treatment with the constructed wetlands, the lead of the raw leachate was found 0.01 ± 0.01 (Ranged from 0.00 mg/ L to 0.02 mg/L). The average zinc (Zn) of the raw leachate was found 1.85 ± 0.21 (Ranged from 1.54 mg/ L to 2.23 mg/ L)

while after dilution the zinc of the leachate was found 1.09 ± 0.13 (Ranged from 0.96 mg/ L to 1.29mg/ L). Our results are in agreement with Agbozu *et al.*,2015 and Gupta and Rani, 2014. After treatment with the constructed wetlands, the zinc of the raw leachate was found 0.31 ± 0.09 (Ranged from 0.20 mg/ L to 0.46 mg/ L). The average copper (Cu) of the raw leachate was found 1.97 ± 0.07 (Ranged from 1.88 mg/ L to 2.12 mg/ L) while after dilution the copper of the leachate was found 0.94 ± 0.07 (Ranged from 0.83 mg/ L to 1.02 mg/ L). After treatment with the constructed wetlands, the copper of the raw leachate was found 0.21 ± 0.04 (Ranged from 0.16 mg/ L to 0.26 mg/ L). The average cadmium (Cd) of the raw leachate was found 0.31 ± 0.10 (Ranged from 0.1 mg/ L to 0.45 mg/ L) while after dilution the cadmium of the leachate was found 0.19 ± 0.07 (Ranged from 0.04 mg/ L to 0.30 mg/v). After treatment with the constructed wetlands, the cadmium of the raw leachate was found 0.07 ± 0.04 (Ranged from 0.00 mg/ L to 0.12 mg/ L). The average iron (Fe) of the raw leachate was found 11.58 ± 1.02 (Ranged from 9.89 mg/l to 12.9 mg/l) while after dilution the iron of the leachate was found 5.40 ± 0.88 (Ranged from 4.24 mg/ L to 6.89 mg/ L). Our results are in agreement with Agbozu *et al.*,2015. After treatment with the constructed wetlands, the iron of the raw leachate was found 1.25 ± 0.24 (Ranged from 0.87 mg/ L to 1.67 mg/ L).

Discussion

The summarized results of raw leachate, diluted and treated leachate were given in Table 4. Table 4 also describes the removal efficiency of *Pistia*

Table 3. Showing Heavy metals concentration in Raw diluted leachate and Treated leachate.

| SPL/PMS | Nickel (Ni) | | Lead (Pb) | | Zinc (Zn) | | Copper (Cu) | | Cadmium (Cd) | | Iron (Fe) | |
|---------|-------------|------|-----------|-------|-----------|------|-------------|------|--------------|------|-----------|------|
| | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW | RW | TW |
| SN-1 | 0.16 | 0.05 | 0.030 | ND | 0.99 | 0.3 | 0.83 | 0.23 | 0.11 | 0.05 | 5.45 | 1.25 |
| SN-2 | 0.13 | 0.05 | 0.029 | 0.01 | 1.23 | 0.39 | 1.02 | 0.19 | 0.21 | 0.09 | 6.89 | 1.67 |
| SN-3 | 0.11 | 0.03 | 0.024 | 0.02 | 1.12 | 0.28 | 0.92 | 0.16 | 0.21 | 0.12 | 4.78 | 1.32 |
| SN-4 | 0.17 | 0.05 | 0.030 | 0.01 | 1.26 | 0.46 | 0.94 | 0.19 | 0.04 | ND | 5.67 | 1.29 |
| SN-5 | 0.12 | 0.02 | 0.022 | ND | 0.98 | 0.22 | 1.01 | 0.26 | 0.2 | 0.04 | 6.51 | 1.56 |
| SN-6 | 0.14 | 0.03 | 0.022 | 0.01 | 0.97 | 0.27 | 1.01 | 0.21 | 0.25 | 0.08 | 5.99 | 1.13 |
| SN-7 | 0.16 | 0.04 | 0.025 | 0.001 | 1.1 | 0.36 | 0.94 | 0.25 | 0.14 | ND | 5.34 | 1.18 |
| SN-8 | 0.13 | 0.04 | 0.031 | 0.011 | 1.01 | 0.2 | 0.83 | 0.18 | 0.23 | 0.06 | 4.45 | 0.98 |
| SN-9 | 0.11 | 0.04 | 0.024 | 0.013 | 1.29 | 0.42 | 0.93 | 0.16 | 0.3 | 0.12 | 4.24 | 0.87 |
| SN-10 | 0.18 | 0.06 | 0.023 | ND | 0.96 | 0.21 | 0.98 | 0.24 | 0.21 | 0.11 | 4.67 | 1.23 |
| AV | 0.14 | 0.04 | 0.03 | 0.01 | 1.09 | 0.31 | 0.94 | 0.21 | 0.19 | 0.07 | 5.40 | 1.25 |
| SD | 0.03 | 0.01 | 0.00 | 0.01 | 0.13 | 0.09 | 0.07 | 0.04 | 0.07 | 0.04 | 0.88 | 0.24 |

stratiotes in the treatment of municipal solid waste leachate in the upwards flows constructed wetland system.

In the case of turbidity removal efficiency of 87.09% was calculated. More or less similar efficiency was also observed by Akinbile *et al.*, 2012 and Mathew *et al.*, 2016. In the case of conductivity, 79.97% removal efficiency was observed. More or less similar efficiency was also observed by Boumechhour *et al.*, 2016. In the case of TSS removal efficiency of 70.54% was calculated. More or less similar efficiency was also observed by Akinbile *et al.*, 2012. In the case of total dissolved solids (TDS) 80.23% removal efficiency was observed. In the case of TS, the removal efficiency of 78.24% was calculated. The solids were removed due to different reactions which results in the coagulation process and reduced the solid content simultaneously turbidity and conductivity were reduced. In the case of pH, the removal efficiency of only 8.24% was calculated. The removal efficiency of 97.58% was calculated in the case of BOD. Nivala *et al.* (2007) also observed more or less similar removal efficiency using an artificial aeration system. Similar removal efficiency was also observed using different plants by various researchers (Lavrova, 2016; Dadrasnia *et al.*, 2017; Wojciechowska, 2017). The removal efficiency of

97.03% was calculated in the case of COD. A more or less similar trend was obtained by Prost-Boucle and Molle, 2012; Akinbile *et al.*, 2012; Lavrova, 2016 and Dadrasnia *et al.*, 2017. In case of some parameters (BOD, COD, and TDS) our results are different from that of the study performed by Gupta and Rani (2014) due to the sampling slot difference (they performed in summer, 2014 while we perform sampling in between summer and rainy season). In summers most of the parameters increased due to evaporation.

In the case, of TKN efficiency removal of 76.41% was calculated. The approximately similar removal efficiency was observed by Axler *et al.*, 2001. Nitrogen removal was due to adsorption on the surface of the substrate. In the present study, less removal was observed in the case of TKN as compared to other studies due to large gravel size contributing to fewer surfaces for adsorption (Wojciechowska *et al.*, 2017; Araya *et al.*, 2016). The removal efficiency of 57.40% was calculated in the case of $\text{NH}_4^+\text{-N}$. Our results are in agreement with Dong *et al.*, 2012; Singh *et al.*, 2016; Akinbile *et al.*, 2012; Dadrasnia *et al.*, 2017. ZhengFang *et al.* (2008), observed 99.90% removal of ammonical nitrogen using immobilized bacteria but in our case, we obtained 57.40% removal due to the absence of artificial adding of mi-

Table 4. Showing characteristics of raw and diluted leachate (Physico-chemical and heavy metals)

| Parameters/ Sampling | Raw leachate (Untreated) | Diluted Leachate (Untreated) | Treated Leachate | % Removal |
|------------------------|--------------------------|------------------------------|------------------|-----------|
| Turbidity | 116.80±13.68 | 57.30±5.54 | 7.40±1.8 | 87.09 |
| Conductivity | 12270.10±413.77 | 9000.60±336.52 | 1803.10±88.5 | 79.97 |
| TDS | 8221.10±272.22 | 6030.40±225.47 | 1192.40±48.7 | 80.23 |
| TSS | 205.90±20.01 | 147.00±226.6 | 43.30±6.6 | 70.54 |
| TS | 8427.00±271.97 | 6177.40±230.52 | 1344.00±35.9 | 78.24 |
| pH | 7.98±0.14 | 7.82±0.12 | 7.18±0.09 | 8.24 |
| BOD | 3421.50±433.58 | 1615.10±77.46 | 39.10±11.97 | 97.58 |
| COD | 12580.10±635.40 | 6274.50±556.15 | 186.30±24.18 | 97.03 |
| TKN | 246.50±21.20 | 141.60±14.12 | 33.40±4.43 | 76.41 |
| $\text{NH}_4\text{-N}$ | 116.40±18.90 | 55.40±11.47 | 23.60±3.63 | 57.40 |
| Chloride | 2787.30±131.90 | 1295.50±79.02 | 504.30±21.68 | 67.03 |
| Nitrates | 41.05±3.18 | 23.25±0.82 | 8.09±0.56 | 65.19 |
| Fluorides | 1.48±0.16 | 0.68±0.07 | 0.28±0.05 | 67.09 |
| T-phosphorous | 32.60±1.99 | 14.03±0.91 | 4.27±0.54 | 69.57 |
| Sulphate | 39.21±1.50 | 22.97±1.16 | 3.24±0.81 | 85.89 |
| Nickel | 0.43±0.03 | 0.14±0.03 | 0.04±0.01 | 70.92 |
| Lead | 0.04±0.01 | 0.03±0.00 | 0.01±0.01 | 71.15 |
| Zinc | 1.85±0.21 | 1.09±0.13 | 0.31±0.09 | 71.49 |
| Copper | 1.97±0.07 | 0.94±0.07 | 0.21±0.04 | 78.00 |
| Cadmium | 0.31±0.10 | 0.19±0.07 | 0.07±0.04 | 64.74 |
| Iron | 11.58±1.02 | 5.40±0.88 | 1.25±0.24 | 76.88 |

crobes to the experiment and other factors as temperature, DO, pH and alkalinity. For the survival of nitrifying and denitrifying bacteria, an optimum amount of dissolved oxygen is necessary (Zhang *et al.*, 2002). In the case of chloride, nitrates, fluorides, and sulfate removal efficiency were 67.03%, 65.19%, 67.09%, and 85.89% respectively.

The removal efficiency of 69.57% was calculated in the case of total phosphorous. More or less similar efficiency was also observed by Akinbile *et al.*, 2012. In the case of lead, copper and cadmium removal were 71.15%, 78.00%, and 64.74% respectively. In the case of a nickel, a removal of 70.92% was calculated. A more or less similar result was obtained by He *et al.*, 2017. In the case of zinc, a removal of 71.49% was calculated. More or less similar efficiency was also observed by Akinbile *et al.*, 2012. In the case of iron removal of 76.88% was calculated. More or less similar efficiency was also observed by Bulc *et al.*, 2006. In the constructed wetlands on the upper layer, a microbial layer known as the Schmutzdecke layer was developed which acts as a biological barrier for the pollutants. Microbes present in this layer eat up all the organic matter present in the inlet water.

Conclusion

Constructed wetlands provide safe and eco-friendly solutions for the management of landfill leachate. Both upward and downward flow CW's are effective but upward flow constructed wetlands are much more effective as it increases the retention time of water in a different layer of the reactor. An increase in retention time increases the efficiency of the present upward flow constructed wetlands with *Pistia stratiotes*. The maximum removal efficiency was observed in the case of BOD (97.58%) followed by COD (97.03%), Turbidity (87.09%) and Sulphate (85.89%). In the case of all the parameters removal efficiency was found more than 60%, except pH (8.24%) and ammonical nitrogen (57.40%). Based on all the parameters studied we can conclude that upward flow constructed wetlands with *Pistiastratiotes* is a good alternative for landfill leachate treatment or wastewater management.

References

- Abood, A.R., Bao, J., Du, J., Zheng, D. and Luo, Y. 2014. Non-biodegradable landfill leachate treatment by combined process of agitation, coagulation, SBR and filtration. *Waste Manag.* 34(2): 439–447.
- Agbozu, I.E., Oghama, O.E. and Akinyemi, O.O. 2015. Physico-Chemical assessment of Leachates Quality in Effluent waste Dumpsite, Southern Nigeria. *Journal of Nigerian Environmental Society (JNES)*. 9(1): 1-11.
- Agdag, O.N. and Sponza, D.T. 2005. Anaerobic/aerobic treatment of municipal landfill leachate in sequential two-stage up-flow anaerobic sludge blanket reactor (UASB)/completely stirred tank reactor (CSTR) systems. In: *Process Biochemistry*, 40(2nd edn): 895-902.
- Akinbile, C.O., Yusoff, M.S. and Ahmad-Zuki, A.Z. 2012. Landfill leachate treatment using sub-surface flow constructed wetland by *Cyperushaspan*. *Waste Manag.* 32 (7) : 1387-1393.
- Araya, F., Vera, I., Sáez, K. and Vidal, G. 2016. Effects of aeration and natural zeolite on ammonium removal during the treatment of sewage by mesocosm-scale constructed wetland. *Environmental Technology*. 37: 1811-1820.
- Axler, R., Henneck, J. and McCarthy, B. 2001. Residential subsurface flow constructed wetlands in northern Minnesota. *Wat. Sci. Technol.* 44 : 345-352.
- Bakhshoodeh, R., Soltani-Mohammadi, A., Alavi, N. and Ghanavati, H. 2017. Treatment of high polluted leachate by subsurface flow constructed wetland with vetiver. *Amirkabir J. Civil Eng.* 49 (1): 43-44.
- Boumechhour, F., Kerbachi, R., Rehoum, A.E. and Benmenni, M.S. 2016. Treatment of partially stabilized landfill leachate using combinations of coagulation, Fenton oxidation and granular activated carbon (GAC) adsorption. *Algerian Journal of Environmental Science and Technology*. 2(3): 249-257.
- Bulc, T.G. 2006. Long term performance of a constructed wetland for landfill leachate treatment. *Ecol. Eng.* 26: 365–374.
- Chen, Y.C., Liu, J., Nie, S. and Wu Wang, D. 2013. Removal of COD and decolorizing from landfill leachate by Fenton's reagent advanced oxidation. *Clean Technol. Environ. Policy*. 16(1) : 189–193.
- Chiemchaisri, C., Chiemchaisri, W., Junsod, J., Threedeach, S. and Wicranarachchi, P.N. 2009. Leachate treatment and greenhouse gas emission in subsurface horizontal flow constructed wetlands. In: *Bioresource Technology*. 100 : 3808-3814.
- Choudhary, A.K., Kumar, S. and Sharma, C. 2011. Constructed wetlands: an approach for wastewater treatment. *Elixir Pollu.* 37 : 3666-3672.
- Dadrasnia, A., Azirun, M.S. and Ismail, S.B. 2017. Optimal reduction of chemical oxygen demand and NH₃-N from landfill leachate using a strongly resistant novel *Bacillus salmalaya* strain. *BMC Biotechnology*. 17:85, DOI 10.1186/s12896-017-0395-9
- Ding, A., Zhang, Z., Fu, J. and Cheng, L. 2001. Biological

- control of leachate from municipal landfills. In: *Chemosphere*. 44(1st edn): 1-8.
- Dong, H.Y., Qiang, Z.M., Li, T.G., Jin, H. and Chen, W.D. 2012. Effect of artificial aeration on the performance of vertical-flow constructed wetland treating heavily polluted river water. *J. Environ. Sci.* 24 : 596-601.
- Gajewska, M., Józwiakowski, K., Ghrabi, A. and Masi, F. 2015. Impact of influent wastewater quality on nitrogen removal rates in multistage treatment wetlands. *Environ. Sci. Pollut. Res.* 22 (17): 12840-12844.
- Gotvajna, A.Z., Tisler, T. and Zagorc-Koncana, J. 2009. Comparison of different treatment strategies for industrial landfill leachate. *Journal of Hazardous Materials*. 162 : 1446–1456.
- Gupta, L. and Rani, S. 2014. Leachate characterization and evaluating its impact on ground water quality in vicinity of landfill site area. *IOSR Journal of Environmental Science, Toxicology and Food Technology*. 8(10): 01-07.
- Gusman, M.S., Andrés, J.M., Abad, M.C. and Ramírez, S.A. 2015. Optimization for Fenton Process in Removal of COD for Landfill Leachate Treatment. *International Journal of Environmental Science and Development*. 6(12): 920-924.
- He, H., Duan, Z., Wang, Z. and Yue, Bo. 2017. The removal efficiency of constructed wetlands filled with the zeolite-slag hybrid substrate for the rural landfill leachate treatment. *Environ. Sci. Pollut. Res.* DOI 10.1007/s11356-017-9402-x
- Hermosilla, D., Cortijo, M. and Huang, C.P. 2009. Optimizing the treatment of landfill leachate by conventional Fenton and photo-fenton processes. *Sci. Total Environ.* 407(11) : 3473–3481.
- Kang, Y.W. and Hwang, K.Y. 2000. Effects of reaction conditions on the oxidation efficiency in the fenton process. In: *Water Research*, 34(10thedn): 2786-2790.
- Klimiuk, E., Kulikowska, D. and Koc-Jurczyk, J. 2007. Biological removal of organics and nitrogen from landfill leachates – A review. In: Pawlowska M. & Pawlowski L. (eds.) *Management of pollutant emission from landfills and sludge*. Taylor & Francis Group, London: 187-204.
- Kumar, P. and Choudhary, A.K. 2018. Constructed Wetlands - A Sustainable Solution for Landfill Leachate Treatment of Latest Technology in Engineering, *Management & Applied Science (IJLTEMAS)* 7(6): 101-106.
- Lak, M.G., Sabour, M.R., Amiri, A. and Rabbani, O. 2012. Application of quadratic regression model for Fenton treatment of municipal landfill leachate. *Waste Manag.* 32(10) : 1895–902.
- Lavrova, S. 2016. Treatment of landfill leachate in two stage vertical-flow wetland system with/without addition of carbon source. *J. Chem. Technol. and Metall.*, 51 (2) : 223-228.
- Mathew, A., Dubey, A. and Mahindrakar, A.B. 2016. Study of Constructed Wetland for Treatment of Landfill Leachate. *Int. J. Chemtech. Res.* 9 (11): 87-95.
- Moravia, W.G., Amaral, M.C.S. and Lange, L.C. 2013. Evaluation of landfill leachate treatment by advanced oxidative process by Fenton's reagent combined with membrane separation system. *Waste Manag.* 33(1) : 89–101.
- Nivala, J., Hoos, M.B., Cross, C., Wallace, S. and Parkin G. 2007. Treatment of landfill leachate using an aerated, horizontal subsurface-flow constructed wetland. *Sci. Tot. Environ.* 380 : 19-27.
- Ntampou, X., Zouboulis, A. and Samaras, P. 2005. Appropriate combination of physico-chemical methods (coagulation/flocculation and ozonation) for the efficient treatment of landfill leachates. In: *Chemosphere*. 62(5th edn): 722-730.
- Ohwoghre–Asuma, O. and Aweto, K.E. 2013. Leachate Characterization and Assessment of Groundwater and Surface Water Qualities Near Municipal Solid Waste Dump Site in Effurun, Delta State, Nigeria. *Journal of Environment and Earth Science*. 3(9) : 126-134.
- Paxeus, N. 2000. Organic compounds in municipal landfill leachates. *Wat. Sci. Technol.* 41 : 323.
- Pedescoll, A., Sidrach-Cardona, R., Sánchez, J.C., Carretero, J., Garfi, M. and Bécares, E. 2013. Design configurations affecting flow pattern and solids accumulation in horizontal free water and subsurface flow constructed wetlands. *Water Res.* 47 (3): 1448–58.
- Prost-Boucle, S. and Molle, P. 2012. Recirculation on a single stage of vertical flow constructed wetland: treatment limits and operation modes. *Ecol. Eng.* 43: 81-84.
- Robinson, H. 2007. The composition of leachates from very large landfills: an international review. *CWRM*. 8 (1): 19-32.
- Saeed, T. and Sun, G. 2012. A review on nitrogen and organics removal mechanisms in subsurface flow constructed wetlands: dependency on environmental parameters, operating conditions and supporting media. *J. Environ. Manage.* 112: 429–448.
- Saubá, K. 2015. Developing constructed wetlands for wastewater reclamation: A review. Master of Science Thesis College of Environmental Science and Forestry. State University of New York, Syracuse, New York, USA.
- Schiopu, A.M. and Gavrilescu, M. 2010. Options for the treatment and management of municipal landfill leachate: Common and specific issues. *Clean, Soil, Air, Water*. 38 (12): 1101–1110.
- Silva, A.C., Dezotti, M. and Sant'Anna Jr., G.L. 2004. Treatment and detoxication of a sanitary landfill leachate. *Chemosphere*. 55 : 207–214.
- Singh, S.K. and Tang, W.Z. 2013. Statistical analysis of optimum Fenton oxidation conditions for landfill

- leachate treatment. *Waste Manag.* 33(1) : 81–88.
- Singh, S., Kaushik, A. and Kaushik, C.P. 2016. Comparing Efficacy of Down-Flow and Up-Flow Vertical Constructed Wetlands for Treatment of Simulated Dumpsite Leachate. *Imperial Journal of Interdisciplinary Research (IJIR)*. 2(8) : 942-945.
- Smaoui, Y., Bouzid, J. and Sayadi, S. 2019. Combination of air stripping and biological processes for landfill leachate treatment. *Environ. Eng. Res.* 2020; 25(1) : 80-87.
- United Nations Environment Programme - UNEP. 2003. Available in: <http://www.unep.org/geo/yearbook/yb2003/070.htm>
- Venu, D., Gandhimathi, R., Nidheesh, P.V. and Ramesh, S.T. 2014. Treatment of stabilized landfill leachate using peroxicoagulation process. *Sep. Purif. Technol.* (129): 64–70.
- Wojciechowska, E. 2017. Potential and limits of landfill leachate treatment in a multi-stage subsurface flow constructed wetland – evaluation of organics and nitrogen removal. *Bioresour. Technol.*, 236: 146-154.
- Wojciechowska, E., Gajewska, M. and Ostojski A. 2017. Reliability of nitrogen removal processes in multi-stage treatment wetlands receiving high-strength wastewater. *Ecol. Eng.* 98 : 365-371.
- Zazouli, M.A., Yousefi, Z., Eslami, A. and Ardebilian, M.B. 2012. Municipal solid waste landfill leachate treatment by fenton, photo-fenton and fenton-like processes: Effect of some variables. *J. Environ. Heal. Sci. Eng.* 9(1): 1-9.
- Zhang, H., Choi, H.J. and Huang, C.P. 2005. Optimization of fenton process for the treatment of landfill leachate. In: *Journal of Hazardous Materials*. 125(1/3th edn): 166–174.
- Zhang, X.L., Peng, D.C. and Wang, Z.Y. 2002. Influence of organic matters on nitrification at low DO in biological turbulent bed reactor. *Chin Water Wastewater (in Chinese)*. 18 (5) : 10-13.
- Zhao Youcai, 2018. Pollution Control Technology for Leachate from Municipal Solid Waste, ISBN-9780128158135,
- Zheng Fang, Y.E., HongYan, Y.U., LiLi, W.E.N. and Jin Ren, N.I. 2008. Treatment of landfill leachate by immobilized microorganisms. *Sci China Ser B-Chem.* 51 (10): 1014-1020.